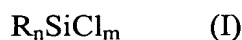


IN THE CLAIMS

Please amend the claims as follows:

Claim 1 (Currently Amended): A process for the preparation of a heterogeneous catalyst active in metathesis reactions of olefins containing rhenium as active component and alumina as inert carrier medium, ~~characterized in that~~ comprising treating the inert carrier is ~~treated~~ with a silanizing agent having the general formula



wherein R represents an amine or a C₁-C₂₅ (iso) alkyl, C₅-C₂₅ cyclo-alkyl, C₆-C₁₈ aromatic or C₇-C₂₅ alkyl aromatic radical, optionally containing at least one heteroatom selected from O, S and N; n is an integer so that 1 < n < 3; m is an integer so that 1 < m < 3.

Claim 2 (Original): The process according to claim 1, wherein the treatment of the carrier is effected using the silanizing agent as such or by means of dissolution of the silanizing agent in a solvent, the alumina being maintained in the presence of the solution of the silanizing agent, for a time ranging from 0.5 to 24 hours, at a temperature ranging from -10 to 100 °C, and subjecting the alumina to optional thermal treatment ranging from 400 to 600 °C.

Claim 3 (Currently Amended): The process according to claim 1 ~~or 2~~, wherein the alumina has a surface area greater than 50 m²/g and a total cumulative pore volume greater than 0.01 ml/g.

Claim 4 (Original): The process according to claim 3, wherein the alumina has a surface area ranging from 100 to 200 m²/g and a total cumulative pore volume ranging from 0.3 to 0.8 ml/g.

Claim 5 (Currently Amended): The process according to claim 1, wherein the active rhenium component is laid on the carrier ~~pretreated as specified in claims 1-4~~, by means of precipitation or impregnation starting from its precursors in the form of solutions of its salts or soluble complexes.

Claim 6 (Original): The process according to claim 5, wherein the rhenium precursors are selected from rhenium heptoxide, ammonium perrenate, tetra-alkyl ammonium perrenate and perrenic acid.

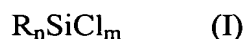
Claim 7 (Original): The process according to claim 1, wherein the catalyst contains a quantity of rhenium ranging from 1 to 20% by weight with respect to the carrier.

Claim 8 (Original): The process according to claim 7, wherein the catalyst contains a quantity of rhenium ranging from 3 to 10% by weight.

Claim 9 (Original): The process according to claim 1, wherein the catalyst containing rhenium on a carrier medium, is activated with a pre-calcination at a temperature ranging from 100 to 200 °C in a stream of dry air and a subsequent calcination at a temperature ranging from 300 to 600 °C first in a stream of dry air and then nitrogen.

Claim 10 (Currently Amended): A process for the conversion of olefins by means of a metathesis reaction ~~characterized in that it is carried out~~ comprising converting olefins in the presence of a heterogeneous catalyst active in metathesis reactions of olefins containing

rhodium as active component and alumina as inert carrier medium, ~~characterized in that~~
wherein the inert carrier is treated with a silanizing agent having the general formula



wherein R represents an amine or a C₁-C₂₅ (iso)alkyl, C₅-C₂₅ cyclo-alkyl, C₆-C₁₈ aromatic or C₇-C₂₅ alkyl aromatic radical, optionally containing at least one heteroatom selected from O, S and N; n is an integer so that 1 < n < 3; m is an integer so that 1 < m < 3.

Claim 11 (Currently Amended): The process according to claim 10, wherein the metathesis reaction ~~can be~~ is homo-metathesis or co-metathesis.

Claim 12 (Currently Amended): The process according to claim 10, wherein the olefins are selected from mono-olefins having from 2 to 30 carbon atoms, cyclo-olefins having from 3 to 20 carbon atoms, polyolefins having from 6 to 30 carbon atoms, and cyclo-polyolefins having from 5 to 30 carbon atoms.

Claim 13 (Currently Amended): The process according to claim 12, wherein the mono-olefins are selected from ethylene, propylene, butene, pentene, and hexene.

Claim 14 (Currently Amended): The process according to claim 12, wherein the cycloolefins are selected from cyclo-pentene, cyclo-octene, and norbornene.

Claim 15 (Original): The process according to claim 12, wherein the polyolefins are selected from 1,4-hexadiene and 1,7-octadiene.

Claim 16 (Currently Amended): The process according to claim 12, wherein the cyclopolyolefins are selected from 1,5-cyclooctadiene, norbornene and dicyclopentadiene.

Claim 17 (Currently Amended): The process according to claim 12, wherein the monoolefins or polyolefins, linear or cyclic, can carry functional groups such as ~~as~~ ~~for~~ ~~example~~, halogens or ester groups such as methyl oleate.

Claim 18 (Original): The process according to claim 10, wherein the metathesis reaction is carried out at a temperature ranging from 0 to 100 °C and a pressure ranging from 0 to 10 MPa (0 to 100 bar).

Claim 19 (Original): The process according to claim 18, wherein the metathesis reaction is carried out at a temperature ranging from 25 to 60 °C and a pressure ranging from 0.1 to 6 MPa (1 to 60 bar).

Claim 20 (Original): The process according to claim 10, wherein the metathesis reaction is carried out in gas phase or in liquid phase with or without a solvent selected from ethers, aliphatic and aromatic hydrocarbons.

Claim 21 (Currently Amended): The process according to claim 20, wherein the solvent is selected from ethyl ether, hexane, heptane, and toluene.

Claim 22 (Original): The process according to claim 10, wherein the quantity of catalyst ranges from 1 to 50% by weight with respect to the reaction mixture.

Claim 23 (Original): The process according to claim 22, wherein the quantity of catalyst ranges from 1 to 10% by weight with respect to the reaction mixture.

Claim 24 (Currently Amended): The process according to claim 10, wherein the metathesis reaction is carried out batchwise or in a continuous manner.